#### ORIGINAL PAPER

# Electroreduction of oxygen at tungsten oxide modified carbon-supported RuSe<sub>x</sub> nanoparticles

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Abstract WO<sub>3</sub>-modified carbon-supported bi-component ruthenium-selenium, RuSex (Ru, 20; Se, 1 wt%), nanoparticles were dispersed in the form of Nafion-containing inks on glassy carbon electrodes to produce electrocatalytic interfaces reactive towards electroreduction of dioxygen in acid medium (0.5 mol  $dm^{-3} H_2SO_4$ ). It was apparent from the rotating disk voltammetric experiments that the reduction of oxygen proceeded at WO<sub>3</sub>-modified electrocatalyst at more than 100 mV more positive potential when compared to bare (WO<sub>3</sub>-free) RuSe<sub>x</sub> system (that had been prepared under analogous conditions and deposited at the same loading of 156  $\mu$ g cm<sup>-2</sup>). The ring-disk rotating voltammetric measurements show that, while the production of hydrogen peroxide intermediate was significantly lower, the kinetic parameter (heterogeneous rate constant) for the oxygen reduction was higher for WO<sub>3</sub>-modified RuSe<sub>x</sub> (relative to bare RuSe<sub>x</sub>). Comparison was also made to highly-efficient Vulcan-supported Pt or Pt/Co nanoparticles: while the half-wave potential for the

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K. S. Nagabhushana · H. Boennemann Forschungszentrum Karslruhe in der Helmholtz-Gemeinschaft Institut fur Technische Chemie ITC-CPV, Karslruhe, Germany oxygen reduction at  $WO_3$ -modified carbon-supported  $RuSe_x$  was still more negative relative to the potentials characteristic of Pt-based electrocatalysts, the oxygen reduction rotating disk voltammetric current densities (measured at 1600 rpm) were almost identical.

**Keywords** Oxygen reduction · Rotating disk voltammetry · Acid electrolyte · Ruthenium–selenium nanoparticles · Tungsten oxide

### **1** Introduction

Fuel cells are becoming an important subject of intense applied and fundamental research. The direct methanol fuel cells (DMFC) have recently attracted interest with respect to possible application as alternative power sources for portable electronic devices [1–4] and vehicles [2, 5]. One of the fundamental problems related to the operation of methanol-oxygen fuel cells is methanol crossover through the polymer membrane from the anode to the cathode compartment where it can be oxidized at potentials also suited for oxygen reduction. The co-existence of both reactions (the reduction of oxygen and the oxidation of methanol) leads to the concomitant depolarization of the platinum cathode. There is a need to search for highly reactive but methanol-tolerant (i.e. selective for the oxygen reduction reaction) electrocatalysts as potential electrode materials for DMFC cathodes.

Although platinum based electrocatalysts are still the most commonly used systems for the reduction of oxygen in acid media, there have been many attempts to synthesize different catalytic materials [3, 4, 6, 7]. Bi-component ruthenium–selenium (RuSe<sub>x</sub>) nanoparticles can be viewed as a promising alternative to Pt and Pt-alloy based cathode

materials. Contrary to Pt type systems, the catalysts utilizing RuSe<sub>x</sub> have been reported to be fully methanol tolerant [8–17]. While bare Ru metal itself is a poor oxygen reduction catalyst, the addition of Se exhibits a profound activating effect. Although there is no unequivocal explanation of the phenomenon of enhancement, a reasonable possibility takes into account chemical stabilization of metallic Ru centers against oxidative degradation through "coordination" of Ru by Se atoms [17].

In terms of current densities, the reactivity of  $RuSe_x$  is pretty high because the system is capable to drive the reduction of oxygen to water as the predominant final product, i.e. with the involvement of almost four electrons and with the formation of only small amounts of hydrogen peroxide intermediate (<5–6%) [15, 18–20, G. Zehl et al. (2006, submitted)]. On the other hand, to make the system competitive to Pt based catalysts, one would have to develop means of activating  $RuSe_x$  catalytic centers to carry out the oxygen reduction reaction at effectively more positive potentials.

In our recent preliminary communication [22], we have reported that modification of carbon-supported RuSe<sub>x</sub> nanoparticles with ultra-thin films of tungsten oxide tends to shift the oxygen reduction potential towards more positive values. Historically, WO3 was found to exhibit powerful catalytic properties towards electroreduction of hydrogen peroxide [23, 24]. In the present work, using rotating ring-disk electrode (RRDE) voltammetry, we address the problem of the formation of H<sub>2</sub>O<sub>2</sub> intermediate at bare and WO<sub>3</sub>-modified RuSe<sub>x</sub> when a moderate loading (ca. 156  $\mu$ g cm<sup>-2</sup>) of the binary electrocatalyst was electrodeposited on glassy carbon disk. The observed lower percent production of hydrogen peroxide, the positive shift of the half-wave potential and the increase in the kinetic parameter (heterogeneous rate constant) clearly imply that modification of RuSe<sub>x</sub> with WO<sub>3</sub> films results in enhancement of the electrocatalytic properties towards electroreduction of oxygen in acid medium (0.5 mol  $dm^{-3}$ H<sub>2</sub>SO<sub>4</sub>). Finally, the activity of the WO<sub>3</sub>-modified RuSe<sub>x</sub> has also been compared to the performance of wellestablished Vulcan-supported Pt and Pt/Co electrocatalysts for the oxygen reduction.

#### 2 Experimental

The electrochemical experiments were performed with CH Instruments (Austin, TX, USA) Model 750A workstation. A mercury/mercury sulfate electrode (Hg/Hg<sub>2</sub>SO<sub>4</sub>), the potential of which was 640 mV more positive relative to the reversible hydrogen electrode (RHE), was used as a reference electrode. This electrode was placed in the second compartment and connected to the main cell through a

Lugging capillary. All potentials are expressed against the RHE.

Rotating disk electrode (RDE) and RRDE voltammetric measurements were accomplished using a variable speed rotator (Pine Instruments, USA). The electrode assembly utilized a glassy carbon disk and a Pt ring. The electrodes were polished with successively finer grade aqueous alumina slurries (grain size, 5-0.05 µm) on a Buehler polishing cloth. In the RRDE measurements, the radius of the disk electrode was 2.3 mm, and the inner and outer radii of the ring electrode were 2.46 and 2.7 mm, respectively. The collection efficiency of the RRDE assembly was determined from the ratio of ring and disk currents (at various rotation rates) using the argon-saturated 0.005 mol dm<sup>-3</sup>  $K_3[Fe(CN)_6] + 0.01 \text{ mol } dm^{-3} K_2SO_4 \text{ solution } [G. Zehl]$ et al. (2006, submitted), 25]. Based on five independent experiments, it was found that, within the potential range considered here, and at rotation rates up to 2500 rpm, the experimental collection efficiency (N) remained unchanged and was equal to 0.23. During the RRDE measurements in oxygen saturated solutions, the potential of the ring electrode was kept at 1.2 V. At this potential, the generated H<sub>2</sub>O<sub>2</sub> is readily oxidized under diffusional-convective control. All RDE and RRDE polarization curves were recorded at a scan rate of 10 mV s<sup>-1</sup>.

All chemicals were commercial materials of the highest available purity (ACS reagent grade) and were used as received. Solutions were prepared from triply distilled subsequently deionized water. They were deaerated (using prepurified argon) or saturated with oxygen for at least 10 min prior to the electrochemical experiment. Experiments were conducted at room temperature ( $20 \pm 0.5$  °C).

Carbon (Vulcan) supported  $RuSe_x$  ( $RuSe_x/C$ ) clusters were fabricated at HMI, Berlin, using the procedure analogous to that described earlier [G. Zehl et al. (2006, submitted)]. In brief, a commercially available Vulcan (XC72) supported Ru (20 wt%) catalyst from ETEK was modified with selenium by its impregnation with an acetonic solution of selenium tetrachloride (SeCl<sub>4</sub>) followed by reductive annealing under forming gas. Their composition of the final material was as follows: Ru, 20; Se, 1; and C 79% (by mass). The diameters of carbon supports and RuSe<sub>x</sub> particles were approximately 20 and 2 nm, respectively. To produce a suspension of bare RuSe<sub>x</sub>/C nanoparticles, a known amount (25 mg) of the catalyst was dispersed in 2 cm<sup>3</sup> of water and subjected to sonication for 10 min. The suspension of WO<sub>3</sub>-modified RuSe<sub>x</sub>/C was produced as follows. A known amount (25 mg) of RuSe<sub>x</sub>/C was dispersed in 2 cm<sup>3</sup> solution of tungstic acid (that had been obtained by passing an aqueous 0.1 mol dm<sup>-3</sup> Na<sub>2</sub>WO<sub>4</sub> solution through a proton exchange resin, Dowex 50 WX2-200). Formation of ultra-thin WO<sub>3</sub> films on RuSe<sub>x</sub>/C occurred through the sol-gel aggregation aging process. As a rule,  $10 \ \mu dm^3$  aliquot of the appropriate suspension was dropped onto the surface of a glassy carbon disk electrode (geometric area,  $0.16 \ cm^2$ ), and the suspension was air-dried at room temperature. The catalyst layer (bare or modified with WO<sub>3</sub>) was subsequently overcoated with Nafion film by adding 3  $\mu dm^3$  of the ethanolic Nafion solution (from Aldrich). As a rule the catalytic films were activated by performing 20–30 full voltammetric potential cycles in the potential range from 0 V to 0.9 V (at 50 mV s<sup>-1</sup>) until steady-state currents were observed. While the morphology of catalytic films was examined using scanning electron microscopy (SEM), the bare and WO<sub>3</sub>-modified carbon (Vulcan)-supported RuSe<sub>x</sub> nanoparticles were first monitored using Philips CM 10 transmission electron microscopy (TEM) operating at 100 kV.

Nanoparticles of carbon (Vulcan XC-72) supported platinum (from ZSW, Ulm Germany) and of carbon (Black Pearl) supported platinum–cobalt ( $Pt_3Co$ ) alloy (from Forschungszentrum Karslruhe, Germany), with the relative metal loadings on the level 40 wt%, were used as comparative catalysts for the oxygen electroreduction. According to the manufacturers' information, the sizes of Pt and Pt<sub>3</sub>Co particles were approximately 2–3 nm. They were deposited on glassy carbon disks in a manner analogous to that described for RuSe<sub>x</sub>/C nanoparticles.

## 3 Results and discussion

Typical TEM images of carbon-supported RuSex nanoparticles RuSe<sub>x</sub>/C, (A) bare and (B) modified with ultrathin layers of tungsten oxide, are illustrated in Fig. 1. The dark dots represent  $RuSe_x$  nanoparticles (Fig. 1A). They have diameters ranging from 2 nm to 3 nm (for brevity, a TEM with larger magnification is not shown here). The lighter areas in Fig. 1A should be attributed to relatively larger (bulk) carbon (Vulcan) supports; they are approximately spherical and tend to form agglomerates (Fig. 1A). But the gravish portions (existing within the lighter areas of Fig. 1B) should reflect the presence of metal oxide  $(WO_3)$ structures in addition to carbon supports. Tungsten oxides seem to be amorphous or polycrystalline, and they overcoat the RuSe<sub>x</sub>/C agglomerates of Fig. 1A. Thickness of WO<sub>3</sub> overlayers is roughly on the level of tens of nm, and it exceeds the size of RuSe<sub>x</sub> nanoparticles.

Figure 2 shows SEM images of  $RuSe_x/C$  nanoparticles, (A) bare and (B) modified tungsten oxide, following deposition in a form of Nafion-containing inks on glassy carbon substrates. In both cases, the catalytic particles form agglomerates on a micrometer scale. But morphology of the WO<sub>3</sub>-modifed system (Fig. 2B) seems to be much denser when compared to WO<sub>3</sub>-free material (Fig. 2A). It is likely that tungsten oxide and/or the mixed Nafion/oxide

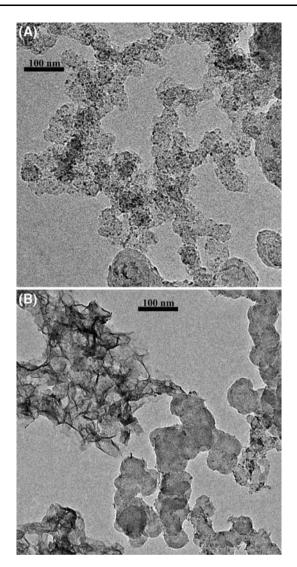


Fig. 1 Transmission electron micrographs of (A) bare and (B) WO<sub>3</sub>modified RuSe<sub>x</sub>/C nanoparticles. While the dark dots represent RuSe<sub>x</sub> nanoparticles, the grayish and light areas stand for carbon supports and tungsten oxide structures, respectively

deposits are filling the void spaces between the  $RuSe_x/C$  nanoparticles.

Figure 3 shows cyclic voltammetric responses of (A) bare, and (B) and WO<sub>3</sub>-modified RuSe<sub>x</sub>/C nanoparticles deposited on glassy carbon electrode and investigated in the deaerated 0.5 mol dm<sup>-3</sup> H<sub>2</sub>SO<sub>4</sub> solution. The main differences between cyclic voltammograms of bare and WO<sub>3</sub>-modified RuSe<sub>x</sub>/C catalysts are as follows. While the bare RuSe<sub>x</sub>/C catalyst is characterized by a fairly flat background response (Fig. 3A), the latter system shows much higher voltammetric currents, particularly below 0.4 V (Fig. 3B), originating from the existence of WO<sub>3</sub> overlayers. Indeed, tungsten oxides undergo reversible reduction to non-stoichiometric oxides, such as substoichiometric hydrogen tungsten oxide bronzes (H<sub>x</sub>WO<sub>3</sub>,

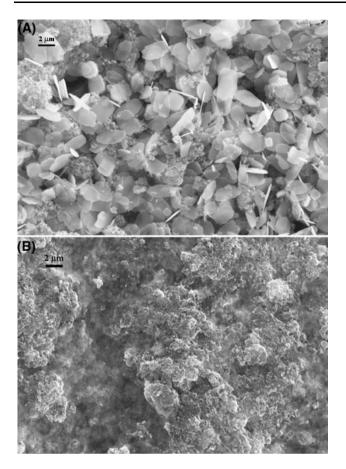


Fig. 2 Scanning electron micrographs of Nafion-treated inks of (A) bare and (B)  $WO_3$ -modified  $RuSe_x/C$  nanoparticles deposited on glassy carbon substrate

0 < x < 1) or lower tungsten oxides (WO<sub>3 - y</sub>, 0 < y < 1) [23, 24] at potentials mentioned above. Finally, the current increases at potentials higher than 0.75 V observed for both bare and WO<sub>3</sub>-modified RuSe<sub>x</sub>/C catalysts (Fig. 3A, B) most likely reflect some oxidation of the Se-covered metallic Ru nanoparticles.

Rotating ring-disk electrode voltammetry was used to study the electrocatalytic properties of the Nafion-treated inks (deposited on glassy carbon disks) of RuSe<sub>x</sub>/C nanoparticles towards the oxygen reduction reaction in the  $O_2$ -saturated 0.5 mol dm<sup>-3</sup> H<sub>2</sub>SO<sub>4</sub> solution (Fig. 4). While current – potential Curves a and b describe disk responses for WO<sub>3</sub>-free and WO<sub>3</sub>-modified catalytic nanoparticles, the Curves **a'** and **b'** refer to the respective ring responses. The results are consistent with the view that the modification of RuSe<sub>x</sub>/C nanoparticles with ultra-thin films of tungsten oxide shifts the half-wave potential of the RDE oxygen reduction voltammogram (Curve b) ca. 100 mV towards more positive values when compared to the potential characteristic of the bare RuSe<sub>x</sub>/C nanoparticles (Curve a). This potential effect is almost perfectly reproducible within  $\pm 5$  mV. Based on numerous experiments

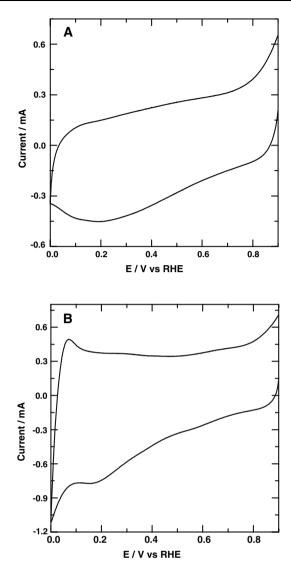
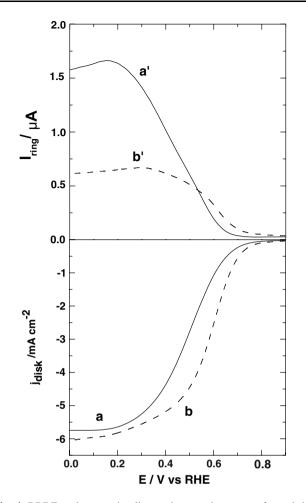


Fig. 3 Comparison of cyclic voltammetric responses of Nafiontreated inks of (A) bare and (B) WO<sub>3</sub>-modified RuSe<sub>x</sub>/C nanoparticles deposited on glassy carbon. Scan rate: 50 mV s<sup>-1</sup>. Electrolyte:  $0.5 \text{ mol dm}^{-3} \text{ H}_2\text{SO}_4$ 

done on various samples, the disk currents, when measured at 0.2 V upon application 1600 rpm rotation rate, are reproducible within 5%. The value of disk current density determined for the WO<sub>3</sub>-modified system (Curve **b**) has been found to be statistically only slightly higher in comparison to the system utilizing bare catalytic nanoparticles (Curve **a**). But ring currents differ much more significantly, clearly implying much more pronounced formation of hydrogen peroxide intermediate (particularly at potentials lower than 0.5 V) in the case of the system containing bare RuSe<sub>x</sub>/C nanoparticles (Curve **a**') relative to the system with WO<sub>3</sub>-modified ones (Curve **b**'). It is apparent from the comparison of the data of Figs. 3B and 4 (Curve **b**') that the relative decrease of the hydrogen peroxide formation starts to occur at potentials where tungsten oxide is



**Fig. 4** RRDE voltammetric diagnostic experiments performed in 0.5 mol dm<sup>-3</sup> H<sub>2</sub>SO<sub>4</sub>, at 1600 rpm, and at 10 mV s<sup>-1</sup> scan rate. While **a** and **b** refer to disk current-potential curves, the ring (Pt) responses are marked as **a'** and **b'** for the measurements done at catalytic layers (deposited on glassy carbon disks) containing bare and WO<sub>3</sub>-modified RuSe<sub>3</sub>/C nanoparticles, respectively. Ring potential, 1.2 V

becoming electroactive, namely where it is reduced to hydrogen bronzes (that are known to be catalytic towards reduction of  $H_2O_2$  [24]). This result implies direct involvement of tungsten oxide overlays (on  $RuSe_x/C$ ) in the oxygen electroreduction reaction. It should be remembered that partially reduced tungsten oxides should also act as good mediators facilitating electron transfers to dispersed  $RuSe_x$  sites. Further, the mixed deposits of  $WO_3$ and Nafion presumably serve as sources of interfacial mobile protons (improved  $H^+$  mobility) that are necessary to support the four-electron reduction of oxygen to water. The latter phenomena may also explain the positive shift in the potential for the electroreduction of oxygen in the system containing  $WO_3$  (compare Curves **a** and **b** in Fig. 4).

To obtain more quantitative information about the relative formation of hydrogen peroxide during RRDE measurements at glassy carbon disk electrodes covered with bare and WO<sub>3</sub>-modified RuSe<sub>x</sub> catalytic centers, the % amounts of  $H_2O_2$  ( $X_{\% H_2O_2}$ ) have been calculated from the data of Fig. 4 by using the following relationship [G. Zehl et al. (2006, submitted), 25]:

$$X_{\text{\%}H2O2} = (200I_{\rm r}/N)/(I_{\rm d}/(I_{\rm r}/N))$$
(1)

where  $I_r$  is ring current,  $I_d$  stands for disk current, and N is the collection efficiency. The approach is based on the assumption that oxygen undergoes reduction according to two parallel mechanisms: 4-electron reaction to water and 2-electron to hydrogen peroxide. Typical results of calculations are displayed in Fig. 5. In the case of both bare and  $WO_3$ -modified RuSe<sub>x</sub> nanoparticles, the production of H<sub>2</sub>O<sub>2</sub> is sizeable at potentials higher than 0.6 V. Under such conditions, the oxygen reduction RDE currents are not well developed yet (refer to Curves **a** and **b** in Fig. 4) because the potentials are not sufficiently negative to effectively drive the oxygen reduction reaction. Nevertheless, the relative formation of hydrogen peroxide is much higher at the catalyst containing  $WO_3$ -free (bare) RuSe<sub>x</sub>/C. At potentials not exceeding 0.6 V, the values of  $(X_{H_2O_2})$ are fairly low, as apparent from Fig. 5, and they are below 2 and 1% for the systems utilizing bare (Curve a) and WO<sub>3</sub>-modified (Curve **b**) catalytic RuSe<sub>x</sub>/C nanoparticles. On the whole, the data of Fig. 5 are consistent with the view that, in the all potential ranges considered here, the relative formation of hydrogen peroxide is lower in the presence of tungsten oxide.

The representative RDE voltammograms recorded at different rotation rates (ranging from 200 rpm to 2500 rpm) for the oxygen reduction at catalytic layers containing (A) WO<sub>3</sub>-free and (B) WO<sub>3</sub>-modified RuSe<sub>x</sub>/C

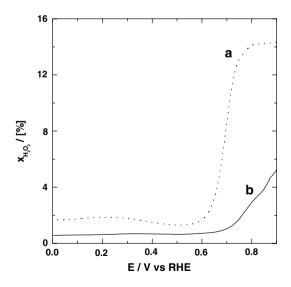
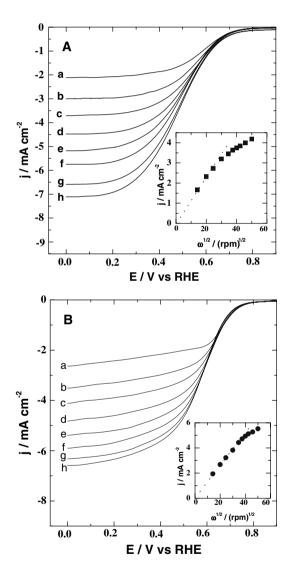


Fig. 5 Fraction of hydrogen peroxide  $(X_{H_2O_2})$  produced during electroreduction of oxygen under the condition of RRDE voltammetric experiment of Fig. 4

nanoparticles are illustrated in Fig. 6. In both cases, the RDE responses are fairly well-defined at any rotation rate studied. Further, half-wave potentials for the reduction of oxygen at the system containing WO<sub>3</sub>-modified RuSe<sub>x</sub>/C (Fig. 6B) are shifted at least 100 mV in the positive direction when compared to those characteristic of the WO<sub>3</sub>-free system (Fig. 6A). The voltammograms of Fig. 6 have been analyzed by the usual means. When the dependencies (Levich type plots) of the RDE current densities (measured at 0.45 V) is plotted versus square root of rotation rates) for electrodes covered with (a) WO<sub>3</sub>-free and (b) WO<sub>3</sub>-modified RuSe<sub>x</sub>/C (Insets to Fig. 5a, b), respectively, deviation from linearity (i.e. from the ideal



**Fig. 6** RDE voltammograms for the oxygen reduction at catalytic layers (deposited on glassy carbon disks) containing (**A**) bare and (**B**) WO<sub>3</sub>-modified RuSe<sub>x</sub>/C nanoparticles. The respective Levich plots of current densities versus square root of rotation rate ( $\omega^{1/2}$ ) for the electroreduction of oxygen (at 0. 45 V) are shown in Insets. Rotation rates: (a) 200, (b) 400, (c) 600, (d) 900, (e) 1200, (f) 1600, (g) 2100, and (h) 2500 rpm. Other conditions as for Fig. 4

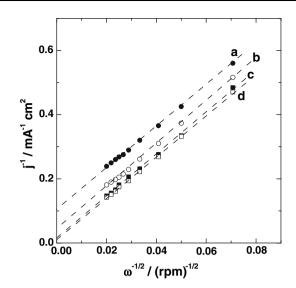


Fig. 7 Koutecky-Levich reciprocal plots (prepared using the data of Fig. 6) for the electroreduction of oxygen (at 0. 45 V) at catalytic layers (deposited on glassy carbon disks) containing (**a**) bare and (**b**) WO<sub>3</sub>-modified RuSe<sub>x</sub>/C nanoparticles. For comparison, the analogous plots are provided for (**c**) Vulcan supported Pt nanoparticles (40 wt%) and (**d**) Vulcan supported Pt/Co nanoparticles. In all cases, the loadings of metallic (bimetallic) catalysts were approximately 150  $\mu$ g cm<sup>-2</sup>

behavior characteristic of systems limited solely by convective diffusion of oxygen in solution) is observed, and seems to be more pronounced at bare rather than WO<sub>3</sub>-modified system. Apparently, the kinetic control is more pronounced, i.e. the catalytic reaction is slower (or less effective) in the case of bare RuSe<sub>x</sub>/C nanoparticles. We have further analyzed the results by means of so called Koutecky-Levich reciprocal plots [24, 25, 27]. Such diagnosis (Fig. 7) is justified because charge (electron, proton) propagation within the catalytic film should be fast, and the oxygen reactant is expected to have easy access to the dispersed active sites (bare or WO<sub>3</sub>-modified RuSe<sub>x</sub>/C nanoparticles). With low amounts of Nafion added to form the inks, any possible limitations related to mass transport through mixed WO<sub>3</sub>-Nafion layers (which may affect the measured current densities) will be considered relatively negligible. We assume that only such factors as transport of oxygen in solution or, at higher rotation rates, the dynamics of the chemical (catalytic) step (reaction) are rate determining. The reciprocal plots (Curves a and b in Fig. 7) have yielded non-zero intercepts clearly indicating kinetic limitations associated with the electrocatalytic film.

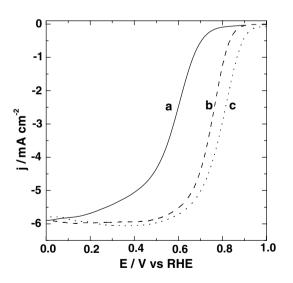
The RDE voltammetric limiting-current densities  $(j_{lim})$  can be expressed as follows [24, 25]:

$$j_{lim}^{-1} = \left( nFkC_{film}C_{Ox} \right)^{-1} + j_L^{-1}$$
(2)

where  $j_L$  is given by the Levich equation (in which the convective diffusion component is proportional to square

root of rotation rate), k is the rate constant for the catalytic reaction in homogeneous units,  $C_{film}$  is the surface concentration of the electrocatalyst, and  $C_{Ox}$  is the bulk concentration of oxygen (1.1 mmol dm<sup>-3</sup> [26]). The symbols *n* and F stand for the number of electrons involved in the process (n = 4) and the Faraday constant. The kinetic parameters can be found from intercepts of the reciprocal plots (Fig. 7). The estimated value of  $kC_{film}$ , which is equivalent to the intrinsic rate of heterogeneous charge transfer, is  $7 \times 10^{-2}$  cm s<sup>-1</sup> for the catalytic electroreduction (at 0.45 V) of oxygen at glassy carbon disks covered with WO<sub>3</sub>-modified RuSe<sub>x</sub>/C nanoparticles (Fig. 7, Curve b). When we performed the analogous determination for bare  $RuSe_x/C$  (Fig. 7, Curve a), the heterogeneous rate constant was found to be  $2 \times 10^{-2}$  cm s<sup>-1</sup>. The above results are reproducible within 5-10% in different experiments. The data simply imply that modification of RuSe<sub>x</sub>/C with ultra-thin layers of WO<sub>3</sub> to the ink results in statistically some (more than three times) increase in the heterogeneous rate constant for oxygen reduction.

Finally, we compared the electrocatalytic performance of WO<sub>3</sub>-modified RuSe<sub>x</sub>/C to the behavior of carbon (Vulcan) supported Pt nanoparticles and carbon (Black Pearl) supported Pt/Co (namely Pt<sub>3</sub>Co) bimetallic nanoparticles deposited on glassy carbon in the form of inks prepared in the analogous manner to those containing RuSe<sub>x</sub>/C. Figure 8 shows the respective RDE voltammograms recorded at 1600 rpm. Although the limiting currents are comparable in all three cases, the half-wave potentials for the electroreduction of oxygen are still ca.



**Fig. 8** RDE voltammetric diagnostic (comparative) measurements performed in 0.5 mol dm<sup>-3</sup> H<sub>2</sub>SO<sub>4</sub>, at 1600 rpm, and at 10 mV s<sup>-1</sup> scan rate. Curves **a**, **b**, and **c** refer to current-potential responses obtained at catalytic layers (deposited on glassy carbon disks) of WO<sub>3</sub>-modified RuSe<sub>x</sub>/C, Vulcan supported Pt (40 wt%), and Vulcan supported Pt/Co nanoparticles

180 or 230 mV more negative in the case of WO<sub>3</sub>-modified RuSe<sub>x</sub>/C (Fig. 8, Curve **a**) when compared to the behavior at Pt (Fig. 8, Curve **b**) or Pt/Co (Fig. 8, Curve **c**). When the  $kC_{film}$  parameters (for the electroreduction of oxygen) were estimated from the intercepts of Koutecky-Levich plots (at 0.6 V) for Vulcan-supported Pt (Fig. 7, curve **c**) and Black Pearl supported Pt/Co (Fig. 7, curve **d**) nanoparticles (deposited on glassy carbon disks), the following values,  $2 \times 10^{-1}$  and  $3 \times 10^{-1}$  cm s<sup>-1</sup> were obtained, respectively. These values are obviously somewhat higher than those determined by us for WO<sub>3</sub>-modified RuSe<sub>x</sub>/C.

In conclusion, the performance of our WO<sub>3</sub>-modified RuSe<sub>x</sub>/C electrocatalyst is lower, in comparison to Pt-based systems, and further research is necessary to find means of further activation of RuSe<sub>x</sub> nanoparticles to shift the oxygen reduction potential towards more positive values. On the other hand, the results clearly show that, by application of such reactive (towards hydrogen peroxide) and protonically/electronically conducting matrix as tungsten oxide [22–24, 28], some enhancement of the oxygen electroreduction at RuSe<sub>x</sub>/C is feasible. There are still possibilities to manipulate the WO<sub>3</sub> thickness and its morphology, as well as to utilize RuSe<sub>x</sub> nanoparticles of different compositions. The related results will be a subject of a future publication.

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#### References

- Kordesch K, Simader G (1996) Fuel cells and their applications. Wiley-VCH, Weinheim
- 2. Wasmus S, Kuver A (1999) J Electroanal Chem 461:14
- 3. Arico AS, Srinivasan S, Antonucci V (2001) Fuel Cells 1:133
- 4. Hogarth MP, Hards GA (1996) Platinum Met Rev 40:150
- Vielstich W, Lamm A, Gasteiger H (eds) (2003) Handbook of fuel cells; A., vol 2. Wiley, Chichester
- 6. Chu D, Gilman S (1994) J Electrochem Soc 141:177
- 7. Heinzel A, Barragan VM (1999) J Power Sources 84:70
- 8. Alonso-Vante N, Bogdanoff P, Tributsch H (2000) J Catal 190:240
- 9. Holze R, Vogel I, Vielstich W (1986) J Electroanal Chem Interfacial Electrochem 210:277
- Bittins-Cattaneo B, Wasmus S, Lopez-Mishima B, Vielstich W (1993) J Appl Electrochem 23:625
- Rodriguez FJ, Sebastian PJ, Solorza O (1998) Int J Hydrogen Energy 23:1031
- Tributsch H, Bron M, Hilgendorff M, Schulenburg H, Dorbandt I, Eyert V, Bogdanoff P, Fiechter S (2001) J Appl Electrochem 31:739
- 13. Chu D, Jiang R (2002) Solid State Ionics 148:591
- Solorza-Feria O, Ellmer K, Giersig M, Alonso-Vante N (1994) Electrochim Acta 39:1647

- Schmidt TJ, Paulus UA, Gasteiger HA, Alonso-Vante N, Behm RJ (2000) J Electrochem Soc 147:2620
- Malakhov IV, Nikitenko SG, Savinova ER, Kochubey DI, Alonso-Vante N (2002) J Phys Chem B 106:1670
- Cao D, Wieckowski A, Inukai J, Alonso-Vante N (2006) J Electrochem Soc 153:A874
- Alonso-Vante N, Solorza-Feria O (1995) Electrochim Acta 40:567
- Paulus UA, Schmidt TJ, Gasteiger HA, Behm RJ (2001) J Electroanal Chem 495:134
- Schulenburg H, Hilgendorff M, Dorbandt I, Radnik J, Peter Bogdanoff S, Fiechter M, Bron H, Tributsch J (2006) Power Sources 155:47
- Zaikovskii VI, Nagabhushana KS, Kriventsov VV, Loponov KN, Cherepanova SV, Kvon RI, Bonnemann H, Kochubey DI, Savinova ER (2006) J Phys Chem B 110:6881

- 22. Kulesza PJ, Miecznikowski K, Baranowska B, Skutnik M, Fiechter S, Bogdanoff P, Dorbandt I (2006) Electrochem Comm 8:904
- 23. Kulesza PJ, Faulkner LR (1988) J Electroanal Chem 248:305
- Kulesza PJ, Grzybowska B, Malik MA, Galkowski MT (1997) J Electrochem Soc 144:1911
- 25. Stamenkovic V, Schmidt TJ, Ross PN, Markovic NM (2003) J Electroanal Chem 554–555:191
- Zecevic SK, Wainright JS, Litt MH, Gojkovic SLj, Savinell RF (1997) J Electrochem Soc 144:2973
- 27. Paulus UA, Schmidt TJ, Gsteiger HA, Behm RJ (2001) J Electroanal Chem 495:134
- Colmenares L, Jusys Z, Kinge S, Boennemann H, Behm RJ (2006) J New Mater Electrochem Syst 9:107